

# Advanced BiCRS Process for H<sub>2</sub> Production with High-Negative Carbon Efficiency – BioVac H<sub>2</sub>™

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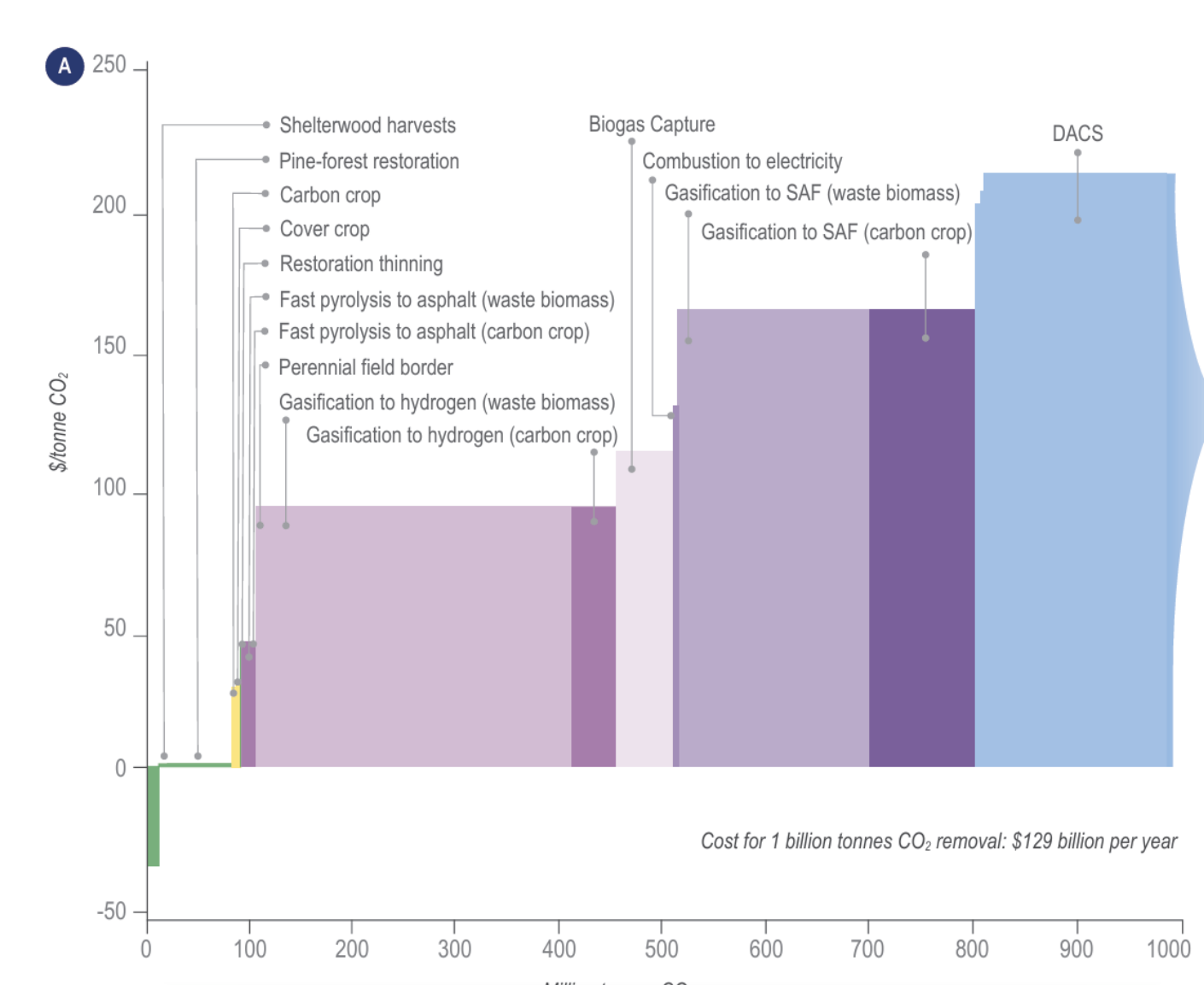
## Motivation and Vision

- BiCRS is a key element of the carbon removal strategy. BiCRS approaches have been evaluated and found to offer a significant potential to meet CO<sub>2</sub> removal (LLNL Roads to Removal, Chapter 6) targets
- Higher C capture and sequestration and higher C negativity are important aspects of a BiCRS process. The BioVac H<sub>2</sub> approach has exceptional performance on this metric along with favorable economics based on early TEA work.

## Benefits and Value

- Removal of CO<sub>2</sub> from the atmosphere while producing energy or chemicals is an important part of global climate strategy.
- This technology can significantly reduce the carbon emissions of BiCRS processes
- Gasification of biomass to H<sub>2</sub> using waste biomass is a large contributor to the low-cost tier of options for CO<sub>2</sub> removal to meet targets
- BiCRS can contribute 350 million tons: per year of needed CO<sub>2</sub> removal

### CO<sub>2</sub> Capture Supply Curve



## Business Concept

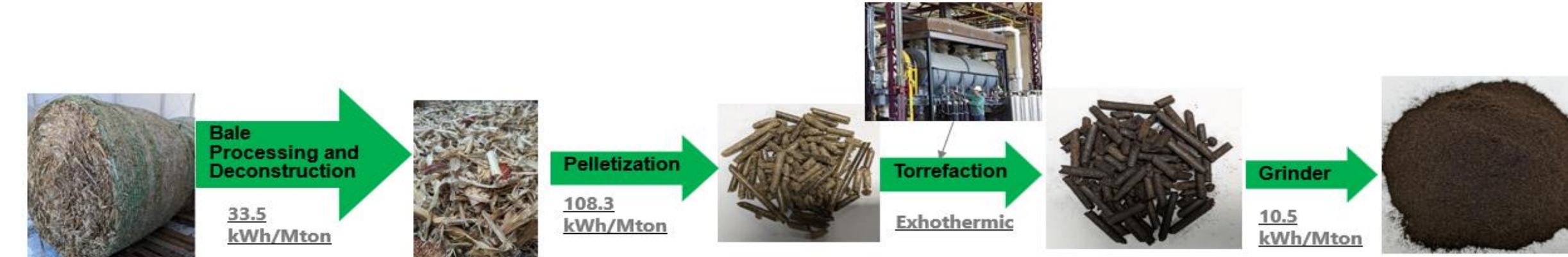
- Develop new BiCRS process, BioVac-H2 using advanced emerging processes

## Technical Solution

- Key features/process
  - Feedstock Pre-processing\*
  - GTI Energy's R-Gas Gasification of Torrefied/Pulverized Ag Wastes\*
  - Water Gas Shift
  - GTI Energy/Uhde GmbH Morphysorb\* AGR solvent – CO<sub>2</sub> Removal and Capture\*
  - Oxy-torrefaction\*
  - Pressure Swing Absorption
  - Power Block – H<sub>2</sub> Combustion/Turbine
  - CO<sub>2</sub> Compression
- \*Developmental Technology

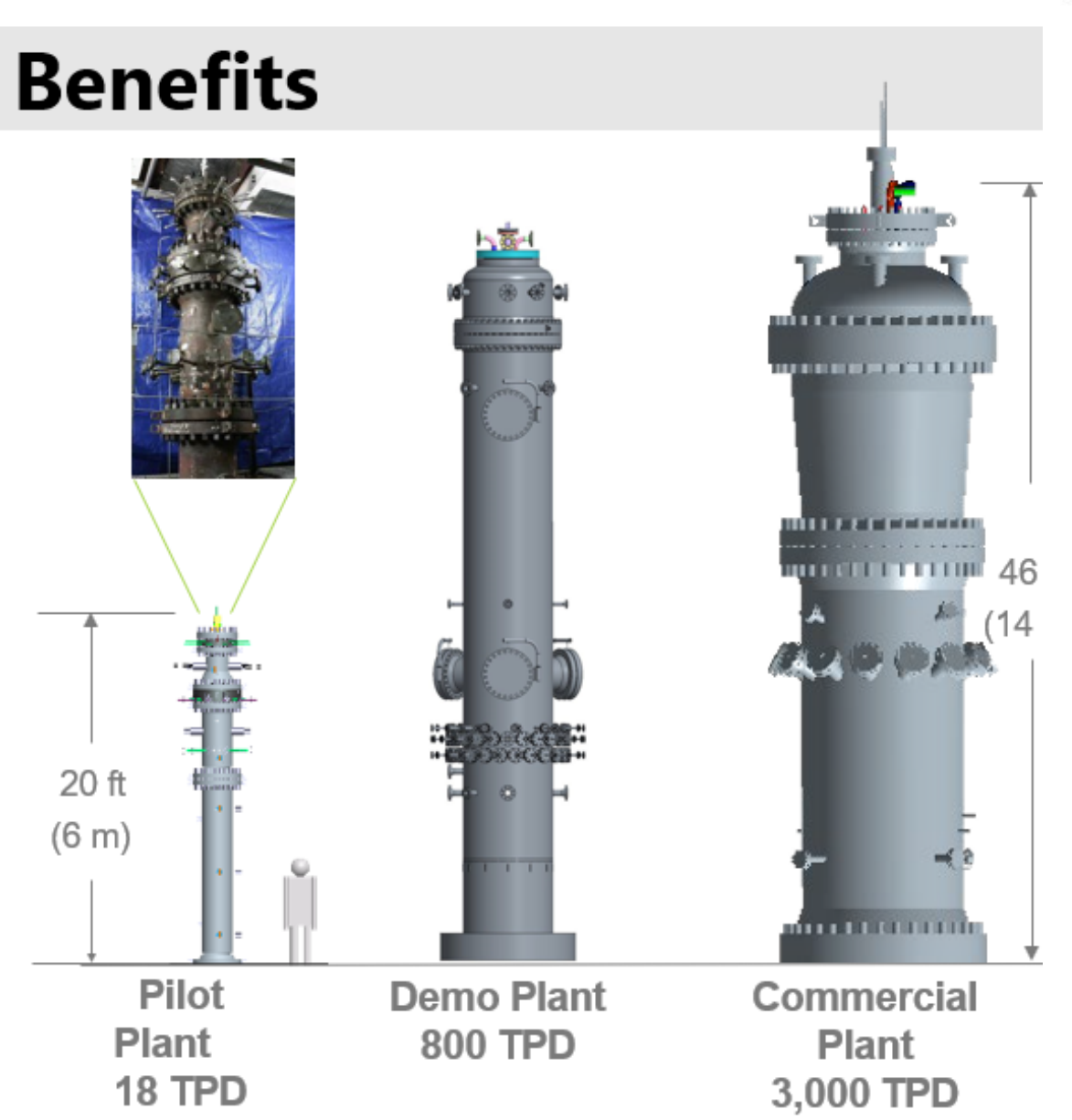
### Feedstock Pre-processing

- Corn Stove (CS) bales are deconstructed and then pelletized.
- The CS pellet torrefaction then go through a torrefaction process at ~245 degC temperature and a residence time of about 30 minutes until the pellet color turns into 'dark brown' inside-and-out with very minimal fibrous materials.
- The feedstock mass loss through the torrefaction process ranges between 10% and 20%.
- The torrefied pellets are then pulverized to achieve a particle size distribution with a median size of about 150 micron.



### GTI Energy's R-Gas Gasifier - Benefits

- High temperature operation enables gasification of high ash fusion temperature and high ash coals
- Efficiency (cold-gas, HHV)
  - 2-4% higher than other dry feed
  - 7-9% higher than slurry
- 15-25% lower CAPEX & OPEX
- Reduced water usage
- 90% smaller reactor volume allows for factory integration, reduce efforts on transportability and maintainability



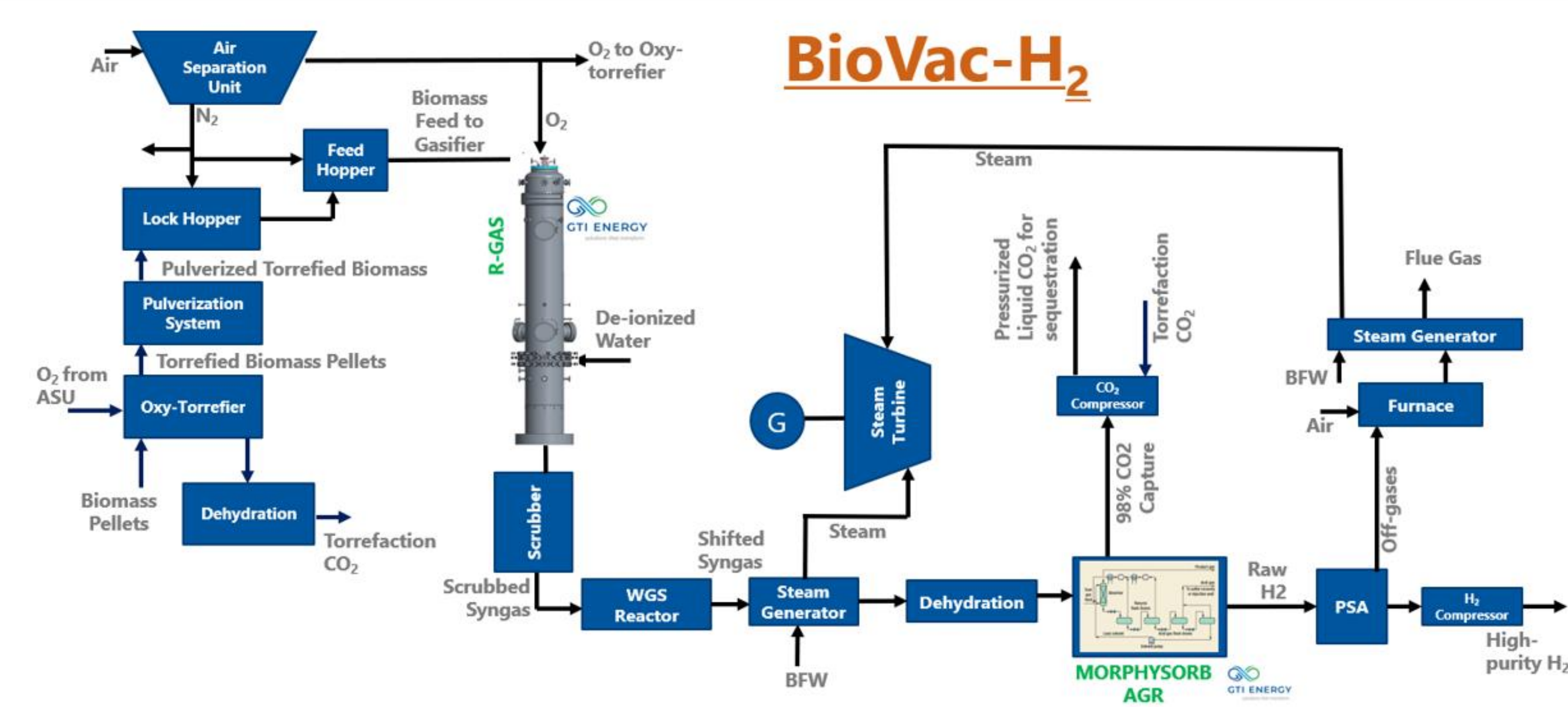
### Acid Gas Removal – Morphysorb® Process

- Solvent process to remove mainly H<sub>2</sub>S and CO<sub>2</sub> from scrubbed syngas.
- Regeneration of rich solvent via flashing with mild heating (if needed.) Lower energy than amine processes.
- Physical solvent – works best at pressure, moderate temperatures (but >50 °F), and in the absence of heavy hydrocarbons
- Tested and developed with natural gas, commercialized for bulk removal of H<sub>2</sub>S and CO<sub>2</sub> (~40 - 50 vol% in total) at ~1,000 psi at 450 MMSCFD.
- Tested in GTI Energy pilot unit (1 MMSCFD) with syngas from fluidized bed gasification of 20 TPD wood in the U-GAS process at ~900 psig.
- Excellent Results in Biomass syngas service (Ref. Acid Gas and Trace Contaminant Removal from Synthesis Gas produced by fluidized bed gasification of wood using the Morphysorb® Process in the GTI Flex Fuel Pilot Plant, D. Leppin, TCBiomass2013, Chicago IL, April 2013)

## Conclusions and Next Steps

- The proposed conceptual process, BioVacH2™, uses advanced biomass feed processing, gasification (R-Gas™), and acid gas treating technology (Morphysorb®) along with state-of-the art CO<sub>2</sub> compression, oxy-torrefaction and power generation equipment (H<sub>2</sub>-capable gas turbines, when available) to convert suitable biomass feedstocks to H<sub>2</sub> or optionally carbon-negative power. Very high pre-combustion CO<sub>2</sub> recovery indicates a very high negative C result for this process.
- Pathway to net-negative H<sub>2</sub> at \$1/kg is REALIZABLE as long as there is a carbon offset market that pays ~\$90/tonne for CO<sub>2</sub> removal.
- GTI Energy will endeavor to continue development of the process depending on available funding. GTI has many of the pilot plant scale equipment modules needed for an integrated test of the concept if the evaluation going forward continues to be favorable.

## BioVac-H2 Block Flow Diagram



## Key Process Advantages

- Torrefaction/ Feed Pre-processing
  - Enables use of various biomass feedstocks with minimal feeding and heavy liquids issues
  - Enables use of entrained flow gasifier with high efficiency, low footprint
- Oxy-torrefaction
  - Torrefaction off-gases combusted at high-temperature in an oxy-combustion system
  - Enables additional CO<sub>2</sub> capture without expensive, massive CO<sub>2</sub> removal from flue gas process
- Gas Turbine
  - Efficient power production with only water vapor emissions. 100% H<sub>2</sub> capable turbines to be available from Siemens and GE around 2030.
- High Efficiency AGR Solvent
  - High CO<sub>2</sub> Recovery, Low regeneration energy (solvent flashing only)

## Key Process Performance Ratios

Parameter	Value
O <sub>2</sub> to C in feed ratio*	1.17
Sales H <sub>2</sub> to C in feed ratio	0.19
CO <sub>2</sub> sequestered, lb/lb C in feed, %	94.7
Net renewable power required, MWe	18

900 tons of biomass per day

79 tons of high-purity H<sub>2</sub> per day → CI < -20 kg CO<sub>2</sub>e / kg H<sub>2</sub>

1,917 tons of CO<sub>2</sub> removal per day

\*Combined O<sub>2</sub> to Gasification and Oxy-torrefaction Feed: Corn Stover

\*\*Additional CO<sub>2</sub> generated from overall process from biomass feed transportation, construction activities – LCA not performed at this time.

## TEA

Capital Costs	
Bare Erected Cost (BEC):	\$ 291,857,396
ASU	\$57,156,697
Biomass Handling and Torrefaction	\$52,097,128
Power Generation	\$ 7,000,000
Gasification Island	\$71,337,088
PSA	\$ 6,266,482
WGS + CO <sub>2</sub> Capture	\$60,000,000
CO <sub>2</sub> Compressor	\$38,000,000
Other direct cost (balance of plant)	\$34,731,030
Indirect Costs (EPCM, spare parts, commissioning etc.)	\$40,860,035
Contingency (15%)	\$55,117,269
Total Plant cost (TPC)	\$422,565,731
Operating Costs	
Biomass (\$70/tonne delivered to site)	\$20,713,896
Hydrogen Revenue (\$1/kg)	\$ (30,763,339)
Chemicals, Catalyst etc.	\$2,000,000
Renewable Power Cost (6 cents/kWh)	\$ 8,798,544
Fixed Annual Cost (Staffing, insurance, maintenance etc.)	\$11,451,315
Total operation cost	\$12,200,415
CO <sub>2</sub> removal cost (\$/tonne)	\$ 88.95

Removal cost is ~\$89/tonne while producing high-purity H<sub>2</sub> at \$1/kg