



Fabrication considerations

For Hydrothermal liquefaction (HTL) plants

Who is presenting?

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- ✓ Chemical engineering degree from University of Waterloo
- ✓ project engineer for various HTL pilot and demonstration plants starting in 2015



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ABOUT ZETON



The world leader in the design and fabrication of pilot plants

- ✓ Canadian company, [founded in 1986](#), Zetron has grown to become the largest designer and builder of pilot plants in the world.
- ✓ Providing Design-Build solutions for pilot plants, including Controls engineering and Factory Testing
- ✓ Serving all major process industries



Zeton in North America

Our facility in Ontario, Canada has seven fabrication bays, totaling over 77,000 ft². These bays are able to accommodate skids up to 48 ft in height.

In addition to standard fabrication bays, Zeton also offers a clean fabrication bay for food and pharma projects.



Zeton Capabilities and Experience | zeton.com



HTL Fabrication Considerations

- Takes place at a combination of **higher pressures** and **temperatures**
- Produces difficulties in fabrication that need to be both taken into consideration in capital cost evaluations and eventually resolved
- Two examples that are the focus of this presentation:
 - A. **Piping Breakpoints** – where does piping go from readily available to heavily customized?
 - B. **Pipe Support Design** – What factors contribute to the difficulties of piping design for HTL plants, and how to resolve them?

PIPING BREAKPOINTS



Quick HTL Introduction

“Underwater Pyrolysis” – Combination of **Decomposition** and **Condensation** Reactions

Temperature range of **250 – 374°C**

Liquid water is involved in the reaction – water must remain in liquid form despite high temperatures

Resultant pressure range of **20 – 250 barg**

Creates medium to high temperature and pressure combination

HTL Pressure/ Temperature Ratings

Consider a reaction temperature of 350°C

164 barg



Boiling Point

+ 35 bar



Operating Margin Above Boiling Point

+ 35 bar



Piping Pressure Losses Upstream

234 barg

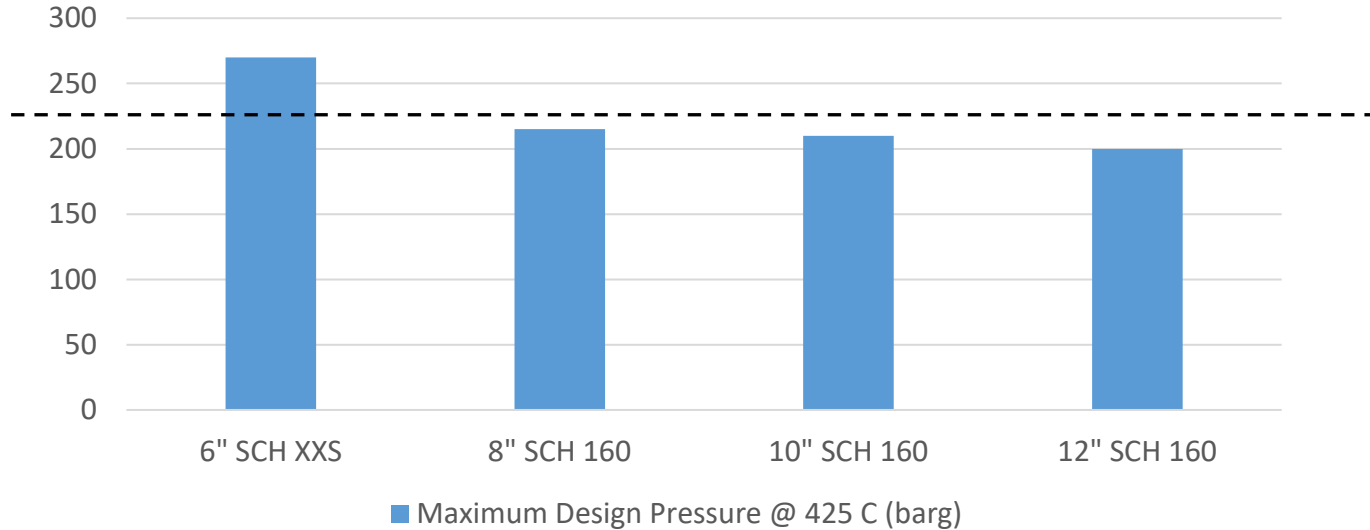


Max Operating Pressure

PUTTING APPROPRIATE DESIGN MARGIN, THIS
CASE PRODUCES DESIGN CONDITIONS OF
260 BARG @ 425°C

Maximum Pipe Ratings

Maximum Design Pressure @ 425 C (barg)



- SS 316/L Pipe
- Assumes no corrosion allowance
- Price difference between 6" SCHXXS and 7" Heavy Wall Tubing, same ID:

3.6X Multiplier on Materials



PIPE SUPPORT DESIGN

HTL Challenges for Pipe Stress Analysis

HTL Plants present a number of challenges when designing pipe and equipment supports

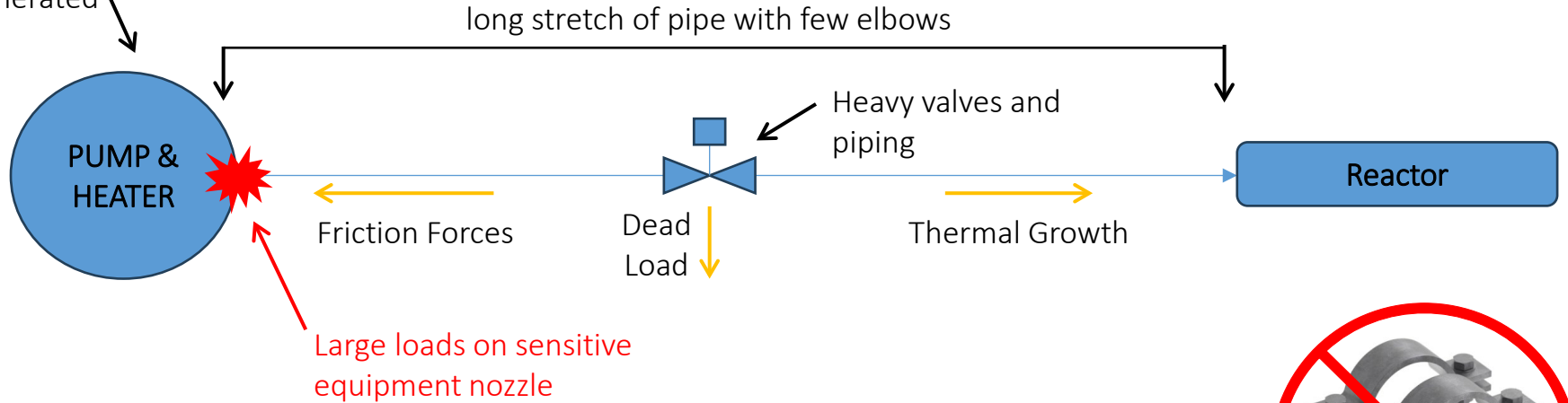
In general, we look to reduce **stress** and increase **flexibility**

High temperatures	→	Thermal expansion	→	Increases Stress
High pressures	→	Thick-walled pipe	→	Decreases Flexibility
Flowing solids	→	Avoid bends	→	Decreases Flexibility
Modular design	→	Tight spaces	→	Decreases Flexibility
Sensitive equipment	→	Low allowable loads	→	Increases Stress

None of these issues are unique on their own, but the **combination** of all these issues often make traditional pipe supports insufficient

Troublesome Loads in an HTL Layout

High pressures and temperatures generated



Typical shoes and sliders are **not sufficient** to support the valves and piping AND allow flexibility to reduce loads.



Custom Solutions Are Complex



Lateral guides

Low friction rollers

Beefy rigid structure



THANK YOU

Questions?